

# Recommendations for an Intensified Monoclonal Antibody Manufacturing Process

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## 1. BACKGROUND

### Project Motivation

- The biopharmaceutical industry is rapidly growing with many companies interested in improving production capabilities to meet speed to market and cost efficiency goals.

### KBI Biopharma

- Contract development and manufacturing organization (CDMO)
- Durham, NC locations focused on the production of monoclonal antibodies (mAbs) with Chinese Hamster Ovary (CHO) cell lines.

### Process Intensification

- Process intensification aims to improve overall manufacturing efficiency by increasing the seeding density of the production culture.
- Requires higher cell densities at the N-1 stage than traditional, low-density processes

## 2. INTRODUCTION

### Goals

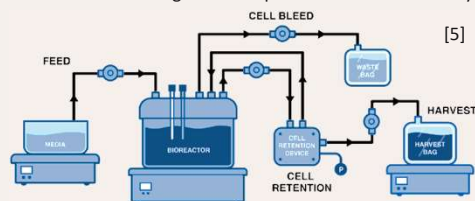
- Recommend a versatile process intensification approach that can be applied to a 2000 L cGMP biomanufacturing plant
- Determine technical and economic feasibility of the recommended process

### Deliverables

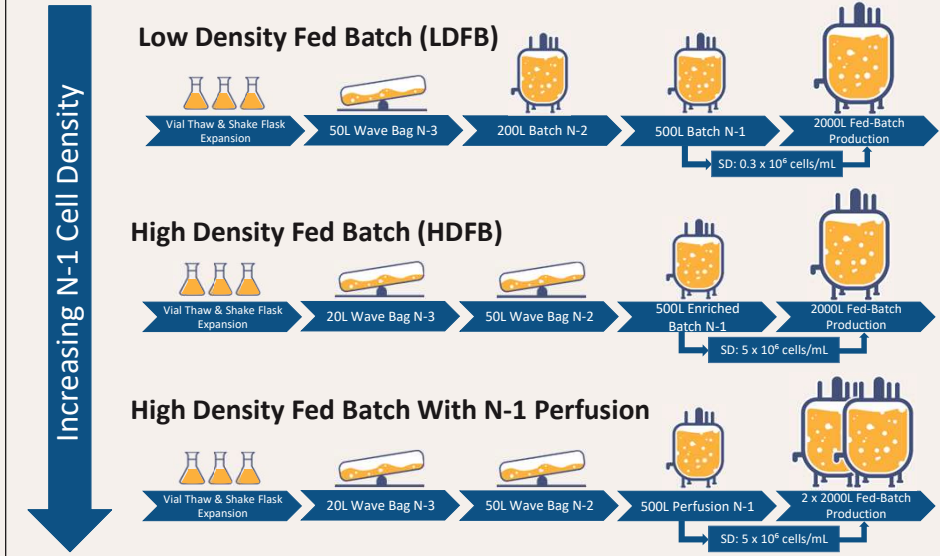
- PFD of recommended process
- Technical specifications for process
- Economic analysis of intensification approaches

### Perfusion Technology

- Perfusion is a mode of continuous bioreactor operation that retains cells through filtration
- Allows for extreme cell densities to be achieved
- Use at the N-1 stage could improve seed train efficiency



## 3. LEVELS OF INTENSIFICATION



## 4. RECOMMENDED PROCESS

### Manufacturing Performance Comparison

Process Type	Expected Product Yield (g/batch)*	Annual Capacity (batches/year)
Traditional LDFFB	10040	20
HDFB	10040	38
HDFB with N-1 Perfusion	10040	76

\*Batch refers to each 2000L production cell culture

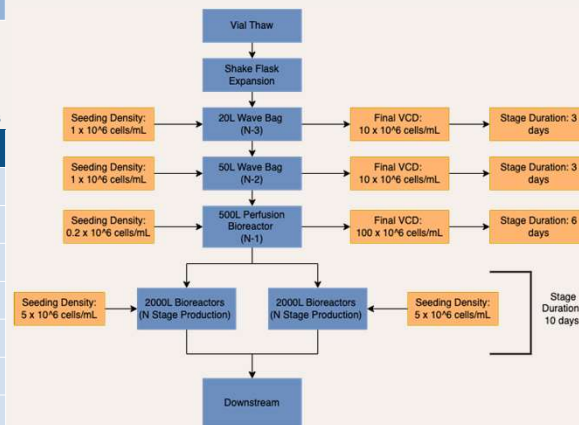
★ Based on our comparison of each level of intensification, we recommend a **High Density Fed Batch Process with N-1 Perfusion**

★ Our proposed process will result in a production stage culture that achieves comparable product titer to a LDFFB process, but with shorter duration batches

★ If N-1 Perfusion is deemed not feasible to implement, our proposed parameters can be applied to a HDFB process with an enriched batch seed

### Suggested Production Culture Parameters

Parameter	Recommended Value
Viability Target for Harvest	70%
pH Setpoint	7.1
DO% Setpoint	60%
Daily Glucose Target	5 g/L
Initial Temperature	36.5°C
Temperature Shift Target	32°C on Day 5
Media Additives	Butyric Acid, Nucleoside, Lysine, Threonine, Tyrosine



## 5. ECONOMIC COMPARISON

### Profit Comparison



### Profitability Analysis Inputs

- Depreciation: Assumes a 6-year lifetime of the capital investment by considering salvage value and the yearly depreciation allowance
- Tax Rate: 45%
- Assumptions: An existing facility is available, 70% yield from harvest to drug product, and all product is sold

### Economic Conclusions

- Revenue: Highest for HDFB with N-1 Perfusion
- Capital Costs: Comparable between LDFFB and HDFB. Highest for HDFB with N-1 Perfusion
- Cost of Manufacturing: Significantly higher for HDFB with N-1 Perfusion
- HDFB with N-1 Perfusion is most profitable**

Approximate Cost (Annual Basis)	Traditional LDFFB	HDFB	HDFB with N-1 Perfusion
Revenue	\$9,000,000,000	\$17,000,000,000	\$35,000,000,000
Capital Cost	\$2,400,000	\$2,400,000	\$3,900,000
Waste Treatment	\$68,000	\$93,000	\$480,000
Operating Labor	\$425,000	\$425,000	\$425,000
Raw Materials	\$8,000,000	\$11,000,000	\$42,000,000
Utilities	\$26,000	\$33,000	\$106,000
COM <sub>1</sub>	\$11,500,000	\$15,500,000	\$54,000,000
Net Profit	\$5,000,000,000	\$10,000,000,000	\$19,000,000,000

## 6. CONCLUSIONS

We recommend the KBI team follow a **reduced duration HDFB with N-1 Perfusion** approach to process intensification. This provides the greatest amount of **profit, productivity, and total product output** while **increasing speed to market**.

## 7. ACKNOWLEDGEMENTS & REFERENCES

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Please scan me for the list of references used! →

