

Green Hydrogen Production Via Steam Methane Reforming

NC STATE UNIVERSITY

College of Engineering

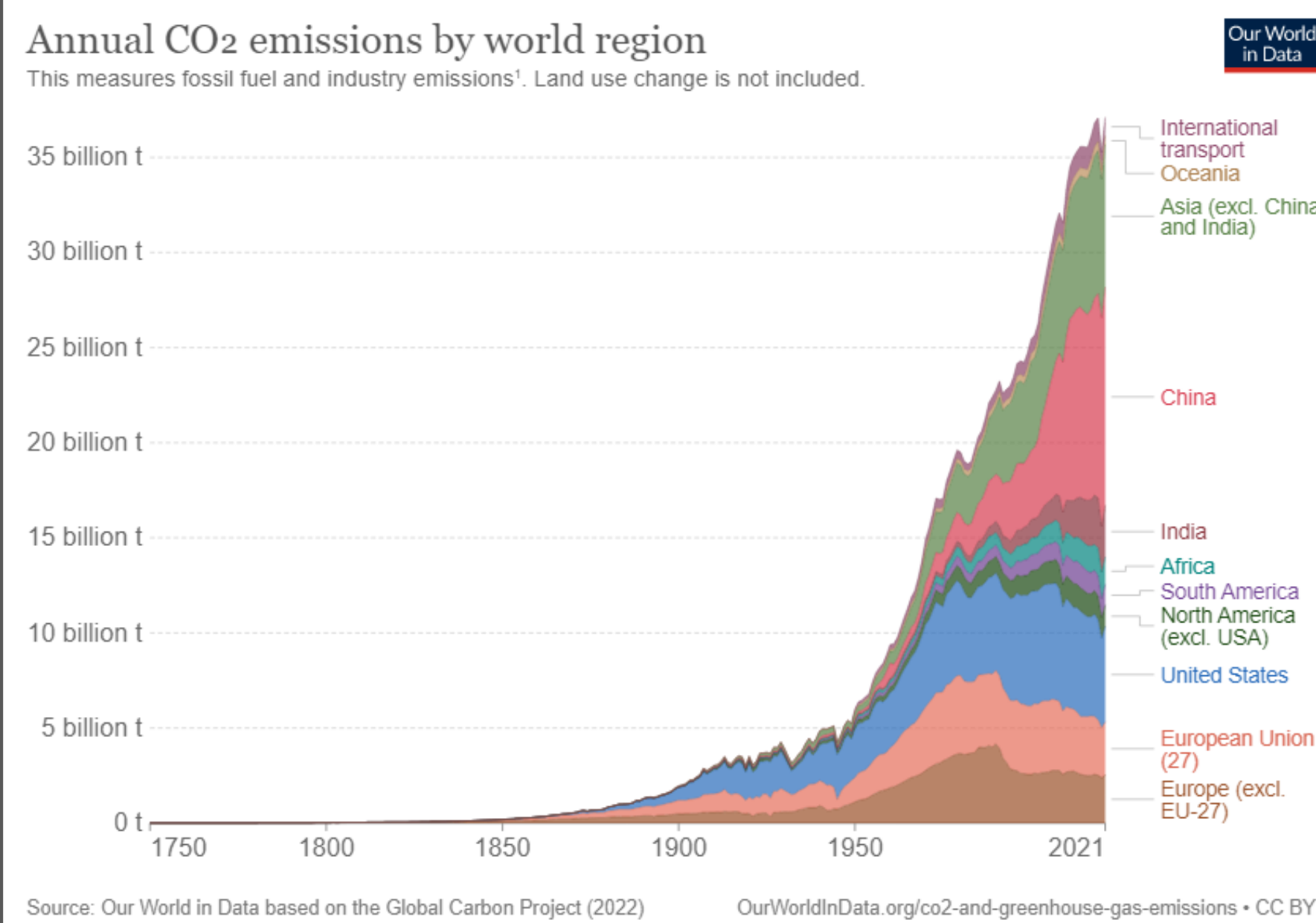
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1. Motivation

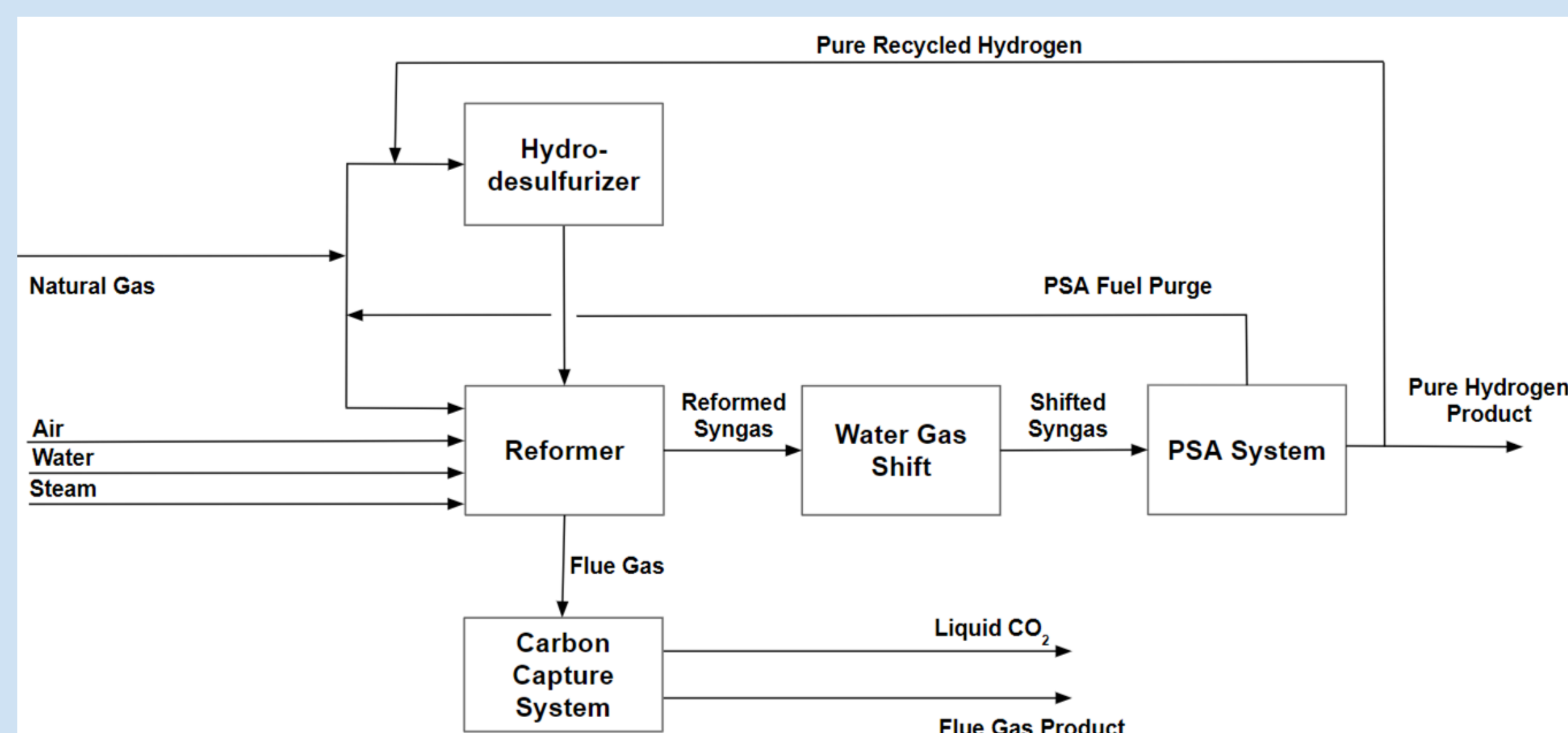
- The imminent climate crisis demands changing our energy infrastructure
- Green Hydrogen produces energy with no carbon emissions, easy to store/transport



2. Project Goals/Capacity

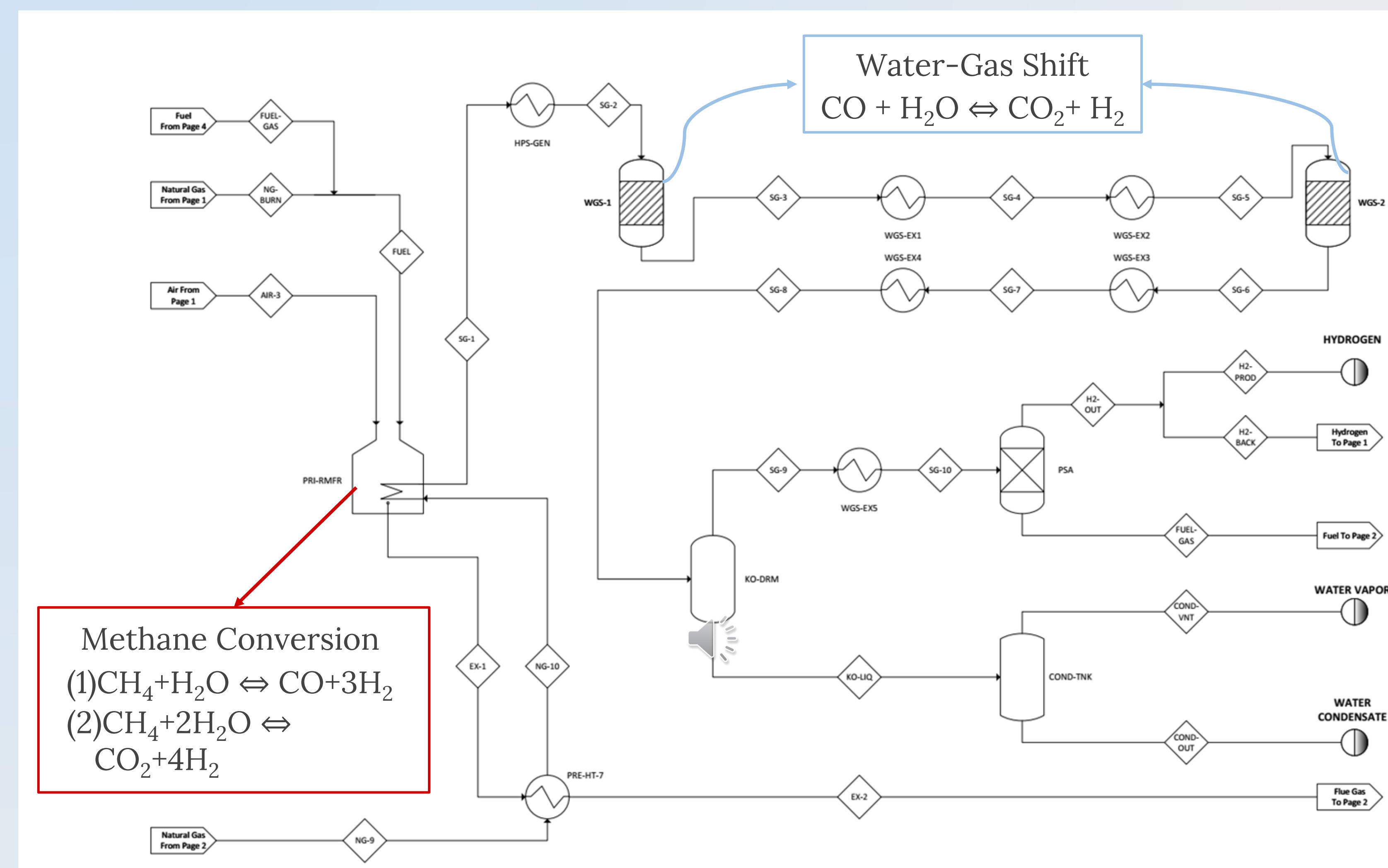
- Develop a Green Hydrogen production facility capable of producing 8.5 kT/yr H₂
- Maximize production efficiency. Minimize cost, carbon footprint

3. Block Flow Diagram



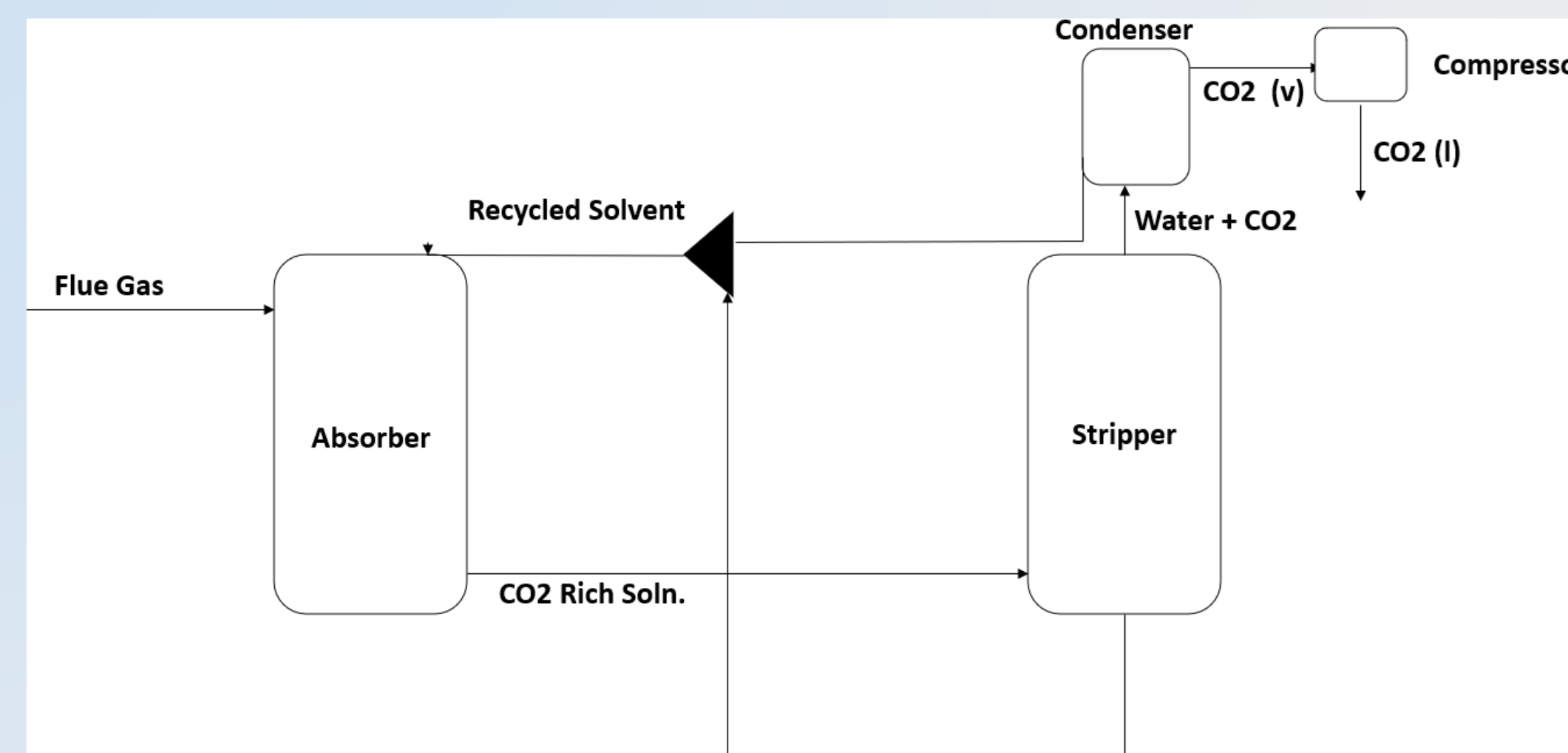
4. SMR Process Design

- Natural gas feed is combined with recycled H₂ product and preheated for desulfurization
- Natural gas stream is mixed with steam to attain a 3:1 steam-to-Carbon ratio for Reformer



- Air and a fuel mixture combust providing heat for endothermic methane conversion
 - Flue gas effluent provides heat for heat exchanger network preheating reformer feeds
- Reformed Syngas effluent passes through shift reactors to increase H₂ conversion
- PSA separates 99.9% pure H₂ final product

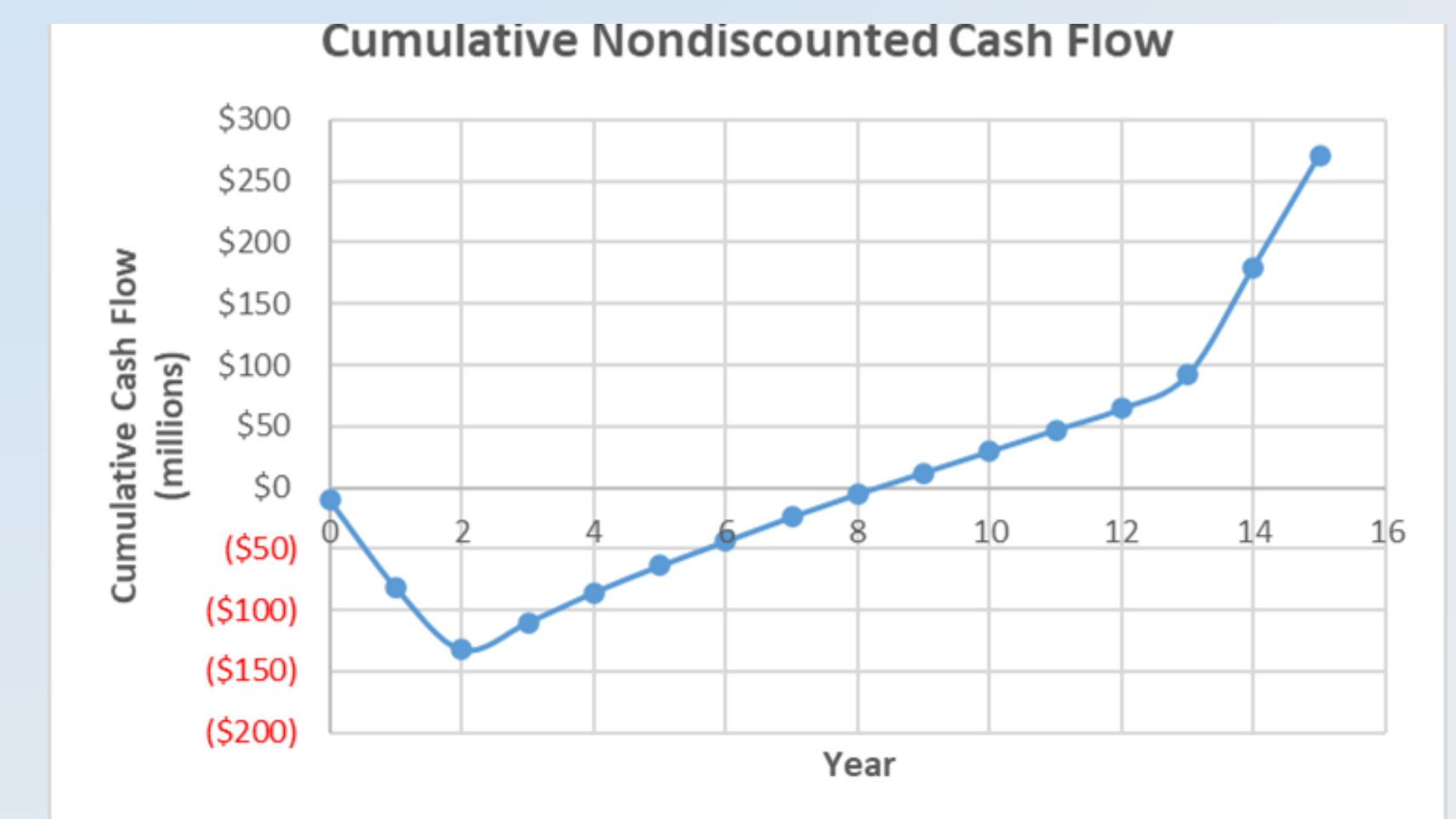
5. Carbon Capture



MEA Based, 90% + Capture Efficiency, located at flue gas stream

6. Economic Analysis

Non-Discounted Values	Discounted Values		
CCP:	+\$271.33 Million	NPV:	+\$121.87 Million
CCR:	2.06	NPW:	1.04
ROROI:	25.33%	DCFROR:	1300000%
		Discount Rate:	10%



	Cost Summary
Capital Cost	\$80,000,000 (-25%) \$107,000,000 \$134,000,000 (+25%)
Cost Manufacturing Without Depreciation	Min: \$28,000,000/yr Median: \$49,000,000/yr Max: \$138,000,000/yr
Total Revenue (Hydrogen and Carbon Dioxide Product)	\$71,000,000/yr

7. CO₂ Emissions

Value	Tons/yr Produced	Tons/yr Captured	Tons/yr Uncaptured
Mass	87000	79000	8000
Percent	100	90.3	9.7

8. Results/Findings

- This SMR plant design would serve as a viable basis for Green Hydrogen production
- Requires adjustments based on the goals of the plant, depending on desired carbon capture goals, production levels