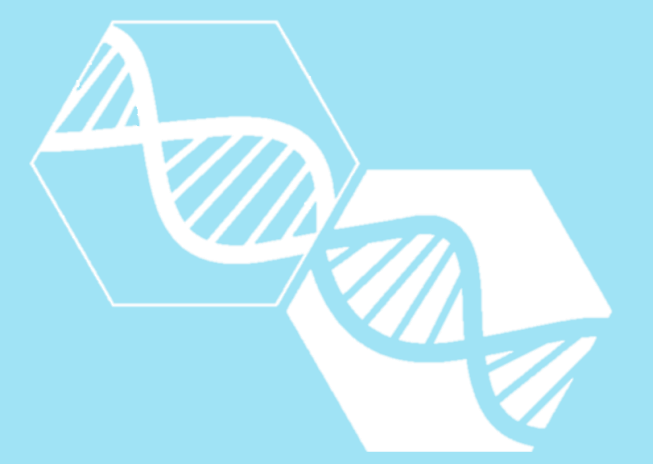


Biofuel Generation via Hydrothermal Processing of Municipal Wastewater Sludge

Andrew Berley, Carmen Jarrell, Lars Wirstrom



I) Motivation

Current Disposal Methods

- Landfill, land application, incineration
- Requires decontamination & dewatering

Concerns

- Regulations & costs (controlling nutrients)
- Emerging contaminants (PFAS)
- Odor, public health & perception

Santa Rosa Water Agency Costs: 27,000 wet tons/year	Composting	Land Application	Landfill
Price per ton	\$150	\$29	\$42



Hydrothermal Processing (HTP)

- High temperature and pressure converts biomass to usable fuels

Benefits

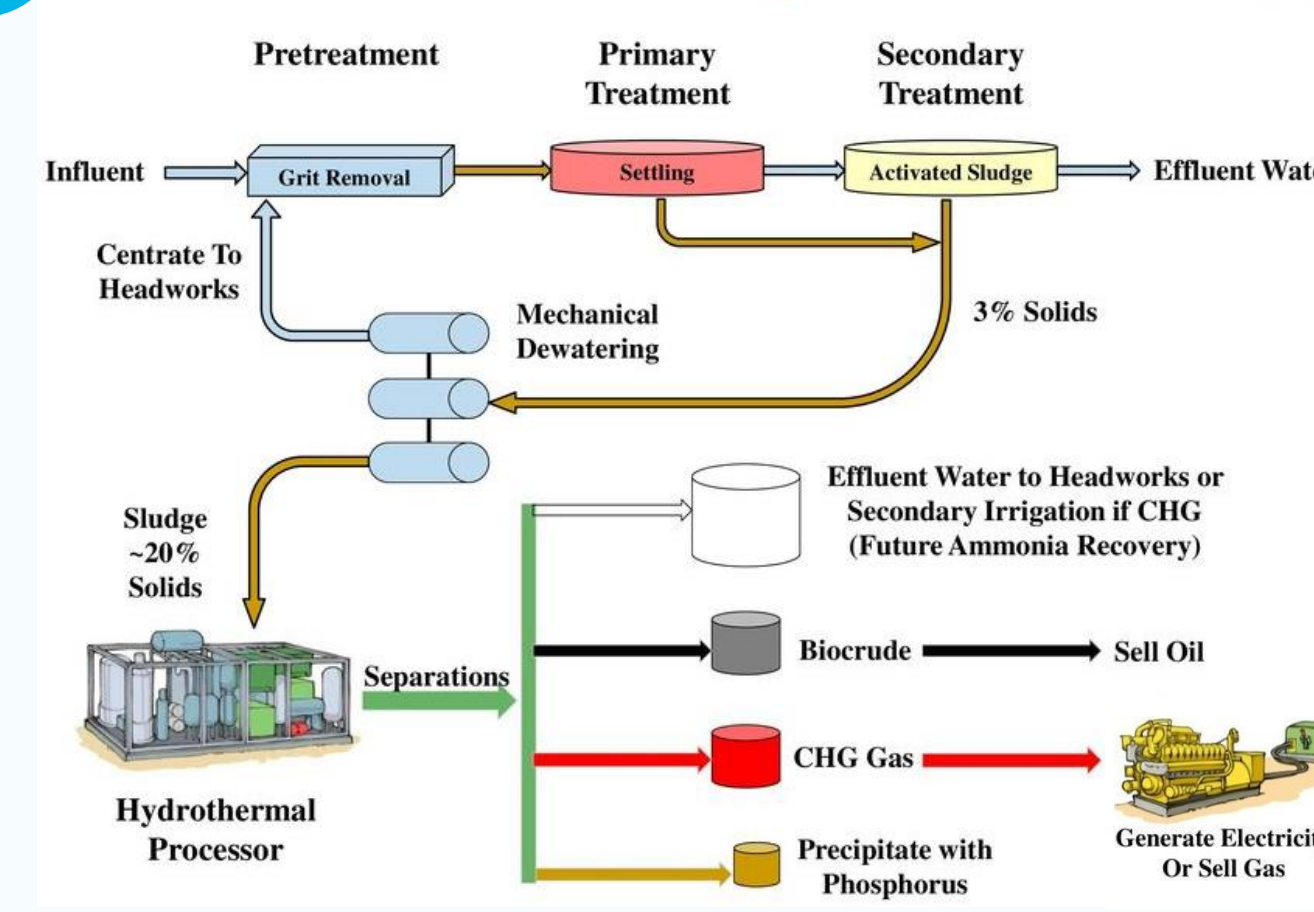
- Solids management
- Low emission
- Resource recovery
- Fuel incentives

II) Goal

Scale up pilot HTP process for 10 dry tons/day wastewater sludge into sellable biocrude keeping in mind:

Economics, Application, Health, Safety, Pollutants & Contaminates, Practicality, and the Environment

WRRF Process Flow with Hydrothermal Processing



V) Economics

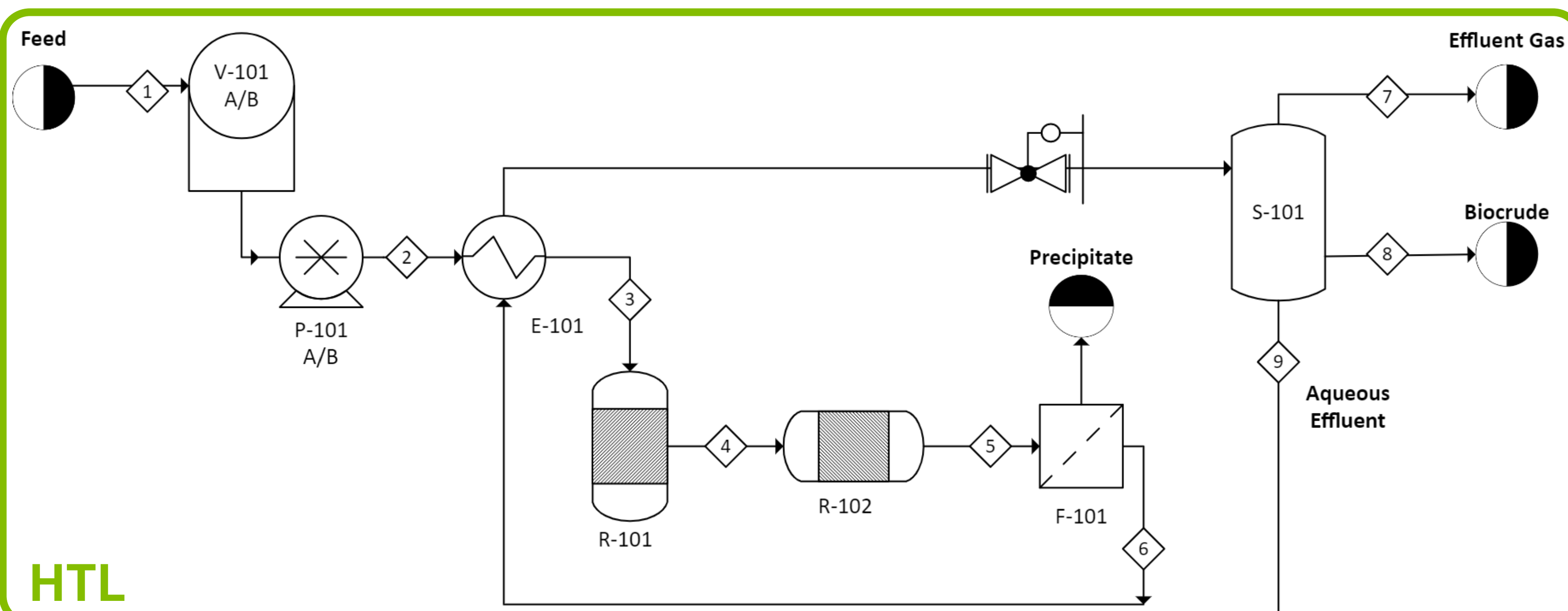
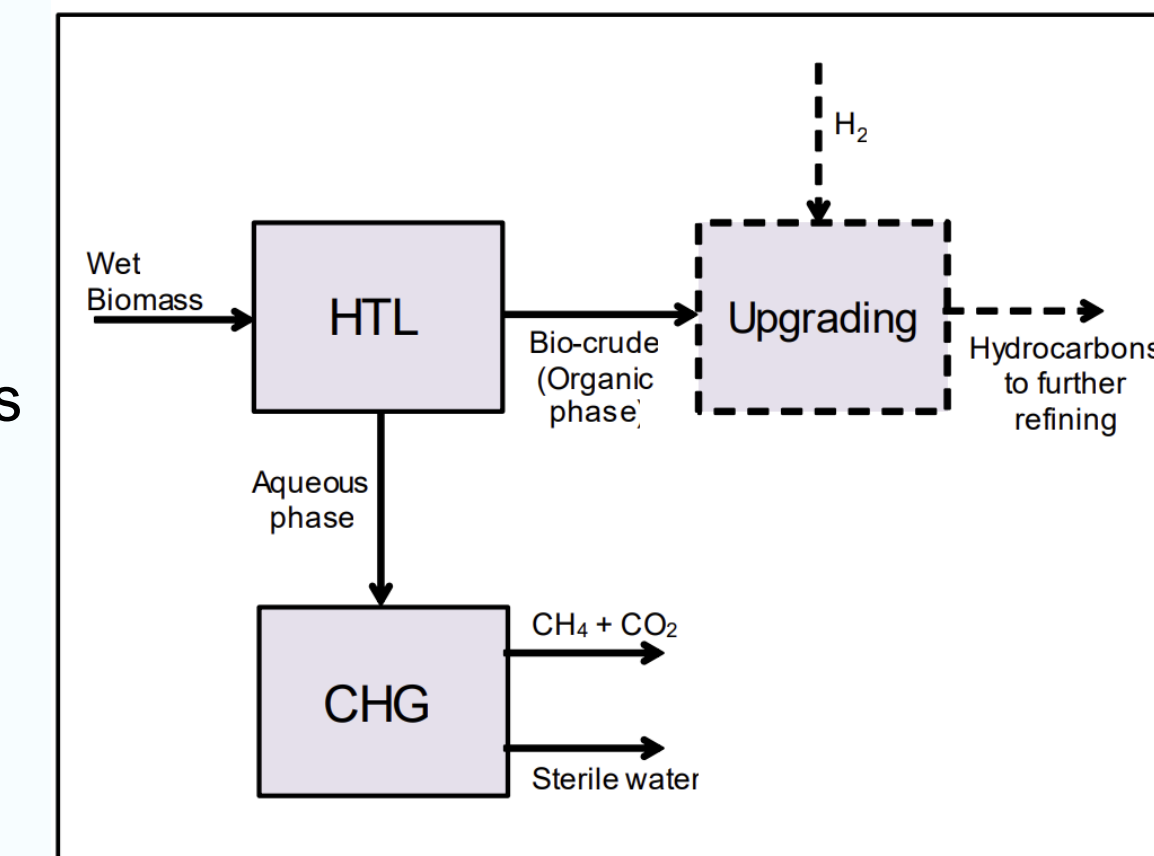
Product Quality

Biocrude:

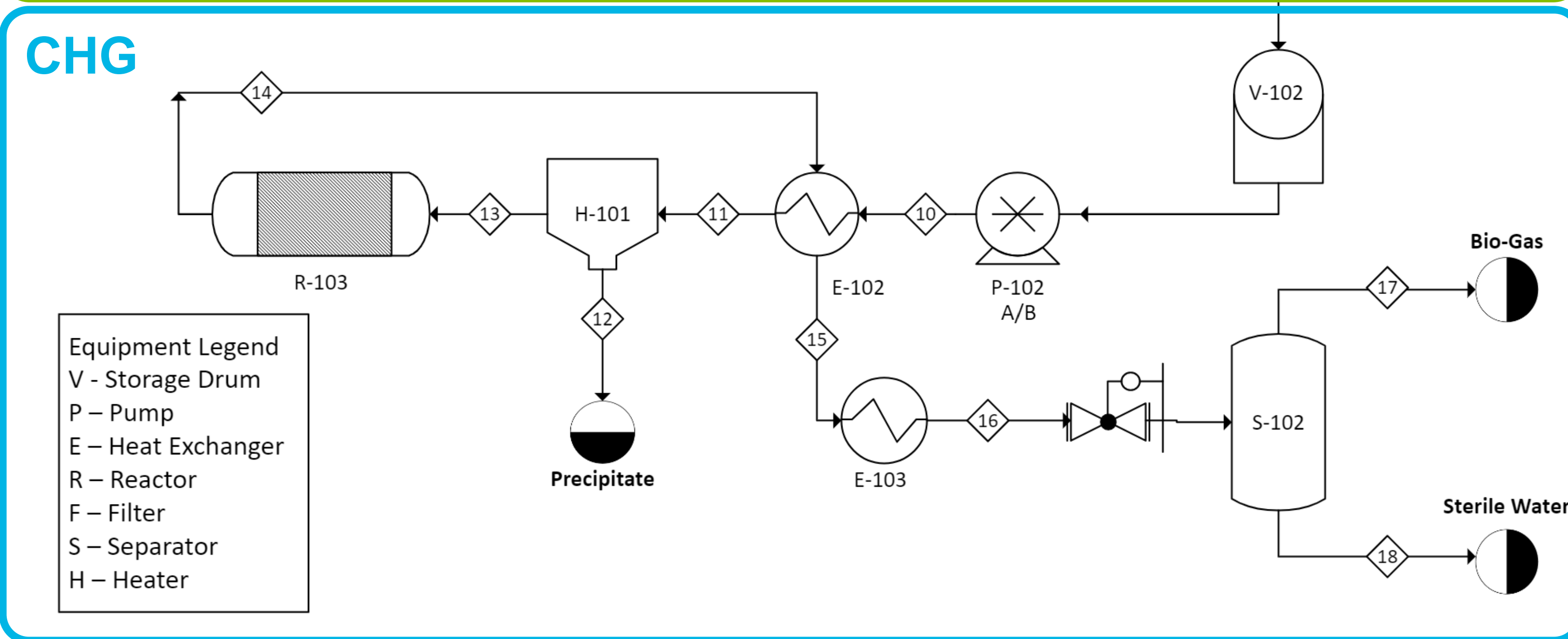
- Comparable to #6 Fuel Oil
- Used for marine diesels and stationary generators
- Upgrade to remove O₂ and ammonia for use in internal combustion engines

CHG Gas:

- Used directly as natural gas



HTL



CHG

- Equipment Legend
- V - Storage Drum
 - P - Pump
 - E - Heat Exchanger
 - R - Reactor
 - F - Filter
 - S - Separator
 - H - Heater

III) Process Design

Feed Mixture: 40:60 primary to secondary sludge and dewatered to 20wt% solids

Process Conditions (PC): 350°C and 2900psig

Assumptions In Heat: CHG feed is water, all sulfur is sulfate

Property	Value	Units
Total Feed Mass Flowrate	96.464	Tonnes/day
Biocrude Mass Flowrate	3.363	Tonnes/day
Aqueous Phase Mass Flowrate	90.515	Tonnes/day
Biocrude Moisture	22.36%	Tonnes H ₂ O/Tonnes Biocrude
Biocrude Ash Content	0.40%	Tonnes Ash/Tonnes Biocrude
Biocrude Yield	29.80%	Tonnes Biocrude/Tonnes Feed
HTL Mass Balance Value*	100.33%	
*Including Gas and Solids production not in table		
Biogas Mass Flowrate	0.487	Tonnes/day
Aqueous Phase Waste Mass Flowrate	90.028	Tonnes/day

Hydrothermal Liquefaction (HTL)

- Heat recycled in E-101 and R-101 is oil heated
- Water approaches critical point → hydrophobic compounds dissolve and inorganic salts precipitate

Catalytic Hydrothermal Gasification (CHG)

- Requires significant heating and cooling water
- Effluent water is cycled back into headworks
- Raney Nickel precedes Ruthenium-Graphite catalyst to prevent sulfur poisoning

Item	Cost over 20 years
Fixed Capital Cost of Equipment	\$250.8 Million
Cost of Operations Labor	\$34.56 Million
Cost of Utilities	\$448.85 Million
Cost of Waste Treatment	\$408.13 Thousand
Cost of Raw Materials	\$44.15 Million
Cost of Manufacture	\$745.88 Million
HTL Biocrude Revenue	\$12.59 Million
CHG Biogas Revenue	\$0.50 Million

Economic Analysis

- Raney nickel and Ruthenium on graphite catalysts are responsible for most of the raw materials cost
- Raney-nickel: \$34.21/kg
- Ruthenium-graphite: \$10,450/kg
- Plant requires 29 operators on staff

VI) Conclusions and Recommendations

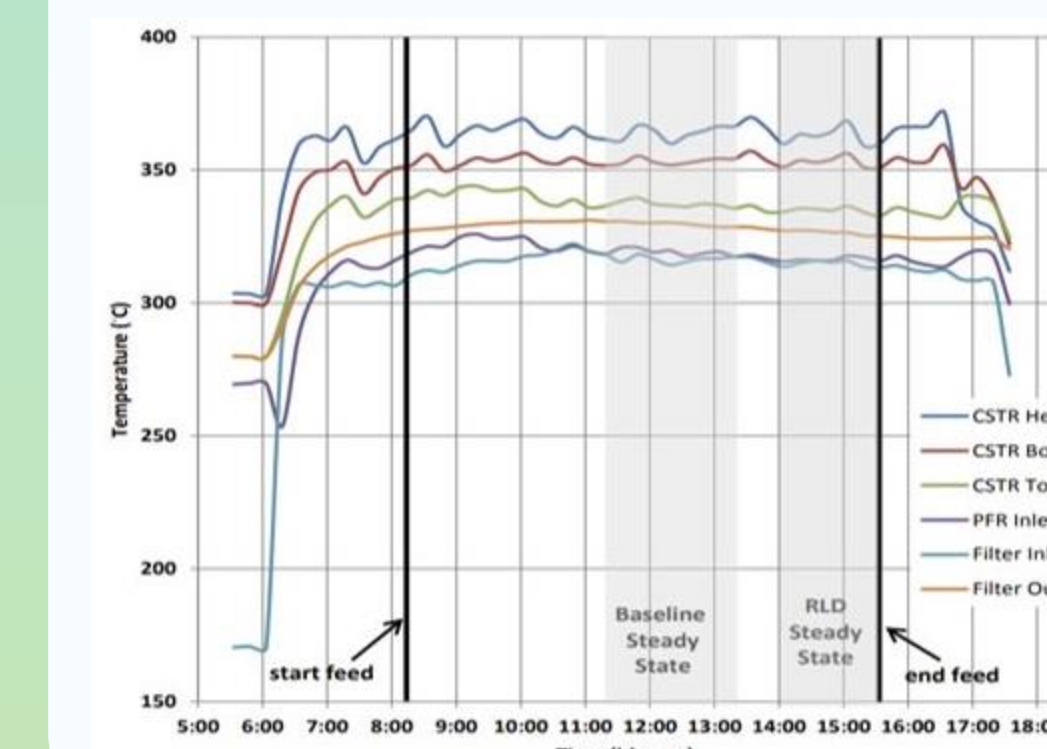
Challenges

- Reaching and maintaining process conditions
- Not enough thermodynamic data for in-depth analysis
- Preventing sulfur poisoning in expensive catalyst



Recommendations

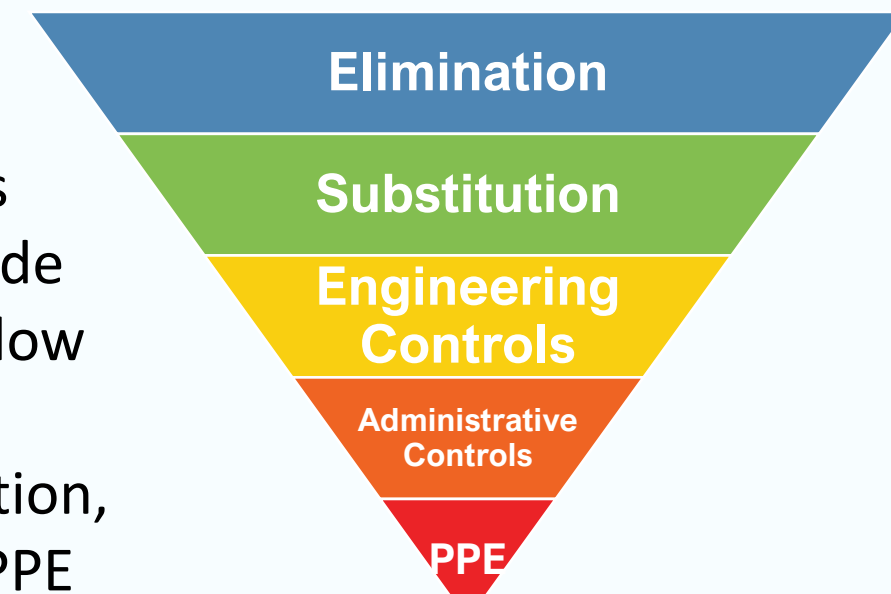
- Research thermodynamics of reactions and HTL organic phase
- Consider alternate uses of precipitate such as fertilizer from high N and P content
- Remove CHG process
- Very costly with little economic return



IV) Safety, Health, and Environmental Concerns

Health & Safety

- Extreme Temperatures and Pressures
- High safety factor
- Personal protective equipment
- Double containment and insulation
- High-grade material of construction
- Sulfur Compounds
- Hydrogen sulfide and sulfate at low concentration
- Proper ventilation, controls, and PPE



High Nitrogen in CHG Aqueous Effluent	High Sulfur Content in HTL gas Effluent	Solid Precipitate positive for Barium and Chromium	Polyfluoroalkyl Substances (PFAS)	Siloxanes
<ul style="list-style-type: none"> • Air stripping • Agricultural discharge 	<ul style="list-style-type: none"> • Air mixing • Scrubber (greener solution) • Ion exchange 	<ul style="list-style-type: none"> • Toxicity characteristic leaching procedure test 	<ul style="list-style-type: none"> • 99% destroyed • Potassium hydroxide additive 	<ul style="list-style-type: none"> • Not present in significant quantities to be concerned

VII) Acknowledgements

Special thank you to our mentor, Mr. Terry Goss and professor, Dr. Lisa Bullard

Citations

Non-cited images are courtesy of the creative commons.
 Lachos-Perez, D., César Torres-Mayanga, P., Abaide, E. R., Zobot, G. L., & De Castilhos, F. (2022). Hydrothermal carbonization and Liquefaction: differences, progress, challenges, and opportunities. *Bioresource Technology*, 343, 126084. <https://doi.org/10.1016/j.biortech.2021.126084>
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