

### Removal of Salt from Wastewater Streams

Caitlin Beckett, Lance Clark, Braxton Coggins, Jordyn Derbes, Mark South Mentor: Dr. Philip McCarter





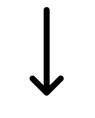
## 1 Motivation and Goals

**Currently:** Nation Ford Chemical processes a wastewater stream with 3,300 mg/L of TDS

**Future:** Implement process that will produce additional stream with 23,083.3 mg/L of TDS

**New Regulation** POTW has proposed a new TDS limit of 1,500 mg/L

#### Goals



 Lower TDS of combined process stream below 1500 mg/L using reverse osmosis



Create an economical separation process



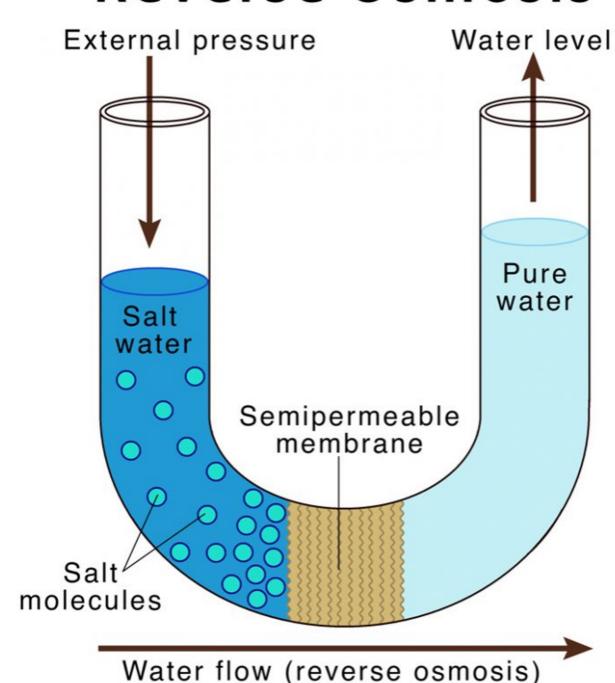
 Minimize safety hazards by implementing control and safety equipment

## 2 Technical Background

**Reverse Osmosis:** pressurized feed ran across membrane configuration.

- Permeate has low concentration of contaminants
- Concentrate has high concentration of contaminants
- Operable range of pressures to satisfy design needs
- Range and bounds found through sensitivity analysis

### Reverse Osmosis



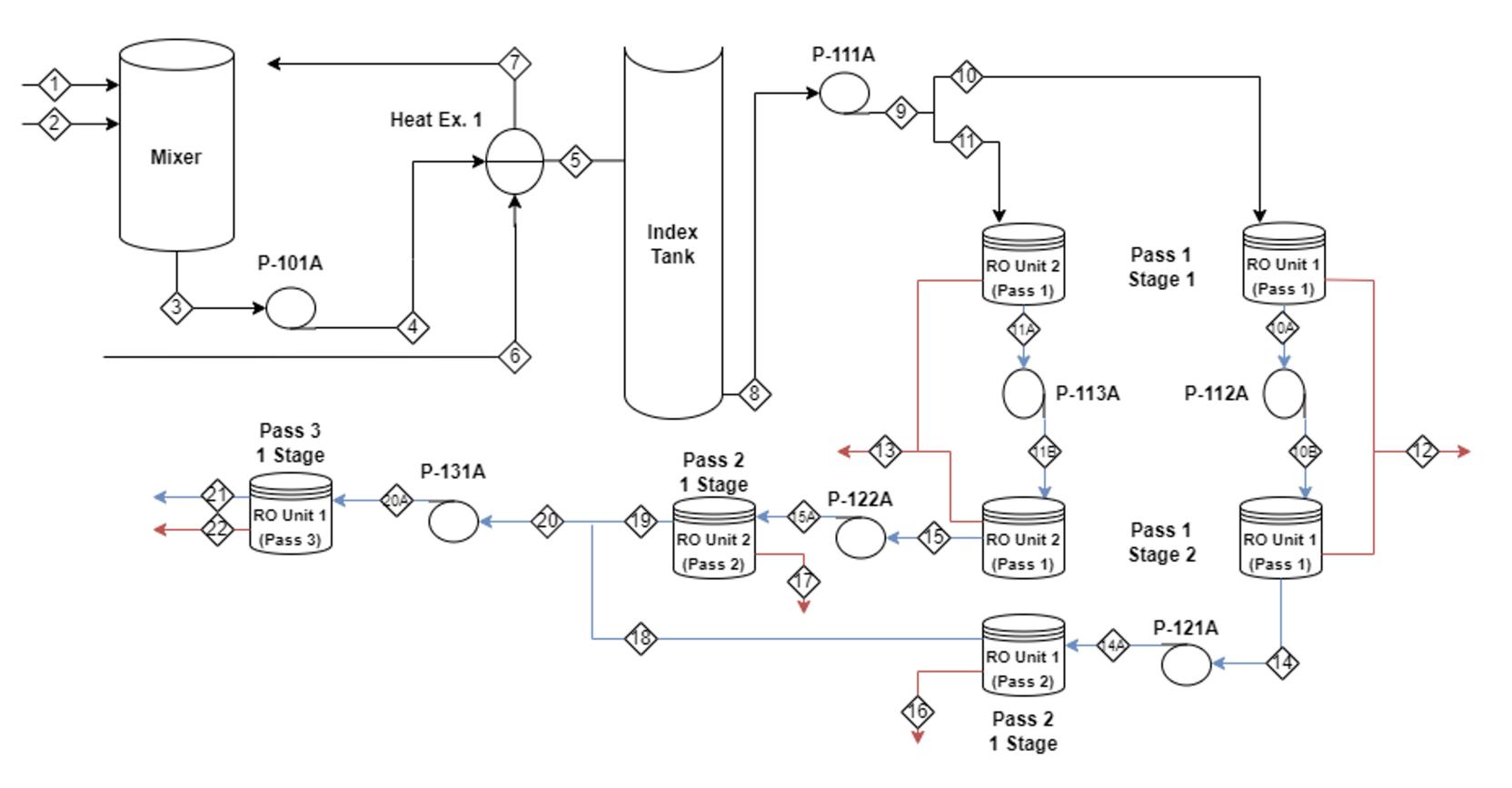
**Reverse Osmosis Diagram** 

Reverse Osmosis, https://www.sciencefacts.net/reverse-osmosis.html

## Design

3

#### **Process Flow Diagram**



### **Equipment Selection**

Equipment Name	Type	MOC			
Mixer	Mixing Tank (built in agitator)	SS 316			
Pumps	Centrifugal	SS 316			
Heat Exchanger	Shell and Tube	Shell: CS // Tube: SS 316			
Valves	Pressure Relief // Globe	SS 316			
Index Tank	Welded Equalization Tank	SS 316			
RO System	FilmTec™ Eco Pro-400 Element	Membrane: Polymer // Housing: SS 316			
Piping	Stainless Steel	SS 316			

#### Stream Table

Otro and Niversia an	40	400	400	4.4.0	40	004	04
Stream Number	10	10A	10B	14A	18	20A	21
Temperature (°C)	21.11	21.11	21.11	21.11	21.11	21.11	21.11
Pressure (psi)	295.00	287.50	295.00	165.00	19.00	19.00	14.70
Flow Rate (gal/min)	8.63	2.07	8.63	6.93	3.31	6.62	0.33
Component Flow Rate (kmol/h)							
Salt 1	0.19	0.04	0.18	0.17	0.01	0.03	0.0008
Salt 2	0.21	0.07	0.31	0.29	0.02	0.05	0.0013
Water	53.78	25.80	107.57	86.22	41.63	83.26	4.15
TDS Mole Percentage	0.73%	0.45%	0.45%	0.21%	0.09%	0.09%	0.05%

#### **Economic Analysis Capital Cost** \$800,000.00 \$755,991.19 \$600,000.00 \$400,000.00 \$200,000.00 SS 316 Small PVC Pipe Material of Construction Final Capital Cost: ~\$756,000 **Operating Cost** Utilities Labor Off-site 72% Maintenance Total Operating Cost: ~\$2,850,000 **Return on Investment** 1<sup>st</sup> Year ROI: ~ -26.3% 3-Year ROI: ~ -32.5%

## 5 Hazards and Operability

# HAZOP Guidewords- *More, Less, No*HAZOP Recommendations

- Use a composition analyzer to determine the effectiveness of the RO separation
- Apply secondary containment such as a dike in the event of loss of containment from an overflow in the index or mixing tanks
- Have regular functionality checks of process equipment
- Add insulation to process piping

## Conclusions

#### The Process is Not Suited for Commercialization

- From a technology standpoint, the project is feasible. RO is widely used in industry.
- To produce half of the volumetric input, there would need to be 27 passes
- The maintenance and energy consumption of so many passes is so expensive that the final ROI will -26.35% after 1 year of operation

### **Acknowledgments and References**

We would like to thank our mentor, Dr. Phillip McCarter, for his time and guidance throughout this project, as well as Dr. Bullard and Dr. Cooper for their teaching expertise.

