# **NC STATE** UNIVERSITY





# **Goals & Motivation**

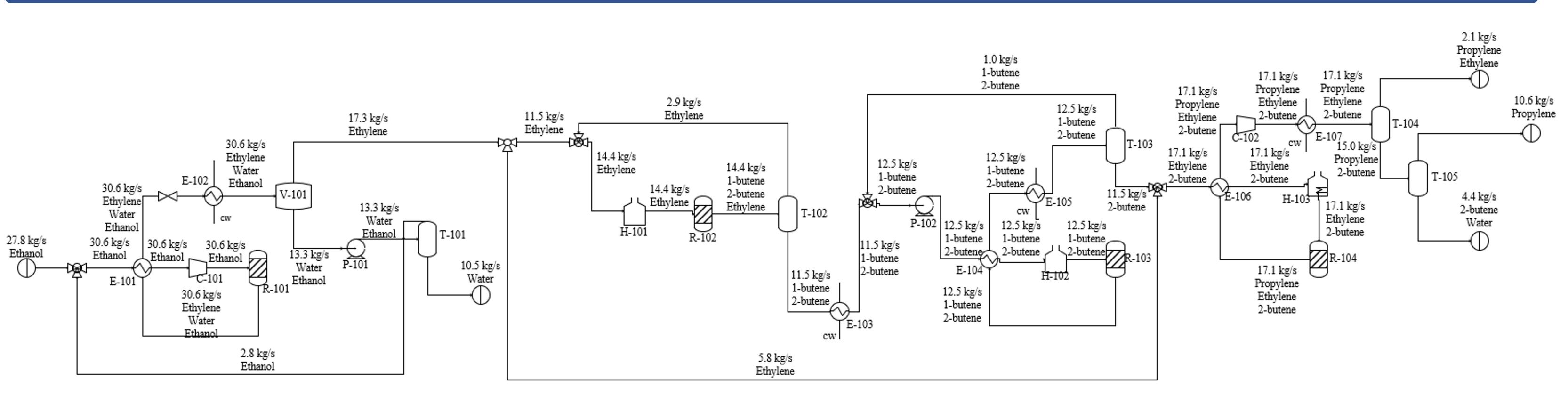
- P&G has a net zero greenhouse gas (GHG) emissions target to reach by 2040.
  - Relevance: Primary consumer of propylene-derivatives (high GHG emissions) to package their products.
- Project Goal: To assess production emissions and costs from biosourced propylene instead of petroleum-sourced.
- Examples of products that P&G develop:

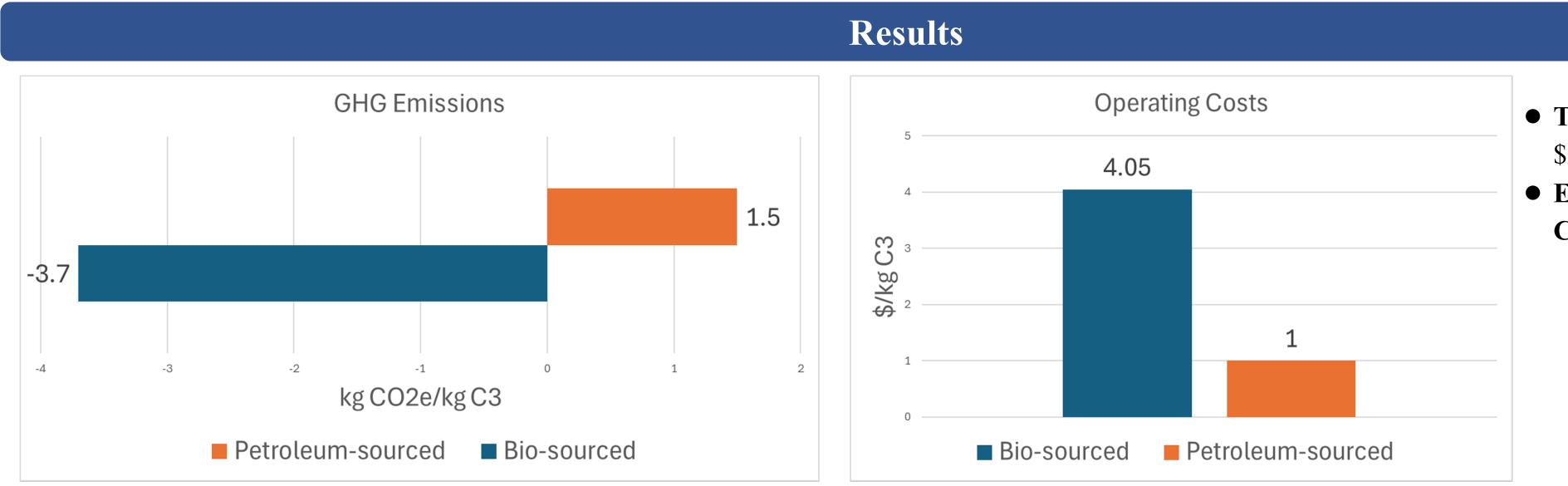


1. Quantify the GHG emissions of propylene produced from ethanol.

Scope

- 2. Quantify the total production cost (TPC) of propylene produced from ethanol.
- 3. Compare the GHG emissions and TPC of bio-sourced and petroleum-sourced propylene.

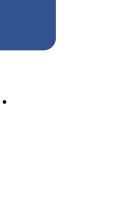




# **Propylene Production from Bio-Ethanol**

P&G Group 2: Davis Brandberg, Aidan Maune, Samantha Walker, Paig April 22, 2024

## **Mass and Energy Balances Mass Balances:** • In = Out• Reaction conversions from industry sources • Basis of 1,000 tons of propylene produced per day (~10.5 kg/s) • Assumed perfect separations **Energy Balances:** • Reactor and separator conditions from industry sources • Reactors $\Delta H_{rxn} = \Sigma (m\Delta H_f)_{out} - \Sigma (m\Delta H_f)_{in}$ • Separators $\Delta S_{mix} = -nR\Sigma y_i ln y_i$ $\Delta G = T \Delta S_{mix}$



| Baseline Ethanol<br>Feed Requirement | 17.6 kg/s    | Model Ethanol<br>Feed Requirement | 27.8 kg/s       |
|--------------------------------------|--------------|-----------------------------------|-----------------|
| Baseline Energy<br>Requirement       | 632 kJ/kg C3 | Model Energy<br>Requirement       | 18,238 kJ/kg C3 |

# **Process Flow Diagram**

- Total Module Cost: \$20.9 million
- Equipment Purchase **Cost**: \$7 million



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| Process Reactions |  |   |  |  |
|-------------------|--|---|--|--|
| Order             | Chemical Formula   | Description                                       |  |  |
| 1                 | $C_2H_5OH \rightarrow C_2H_4 + H_2O$                       | Dehydration of ethanol to ethylene and water.     |  |  |
| 2                 | $2C_2H_4 \rightarrow C_4H_8$                               | Dimerization of ethylene to 1-butene.             |  |  |
| 3                 | $\swarrow C_4 H_8 \rightarrow C_4 H_8 / \square \setminus$ | Isomerization of 1-butene to 2-butene.            |  |  |
| 4                 | $C_4H_8 + C_2H_4 \rightarrow 2C_3H_6$                      | Metathesis of 2-butene and ethylene to propylene. |  |  |
|                   |  |   |  |  |

## **Process Model**

- Modeled in Aspen Plus software
  - Used heaters, heat exchangers, and compressors to achieve ideal conditions
  - Used reactors to achieve new chemical species
  - Used distillation columns and flash tanks to achieve separations
- Model provided mass flows and heat and electricity requirements

# Conclusion

- Make the transition from petroleum to bio-sourced propylene
- Higher cost is necessary to meet net zero GHG emissions target
- Opportunity to lower total module cost through process optimization in the future

# Citations

Scan QR code for a complete list of references.

